



# Integrated Electrochemical Systems for Scalable CO<sub>2</sub> Conversion to Chemical Feedstocks

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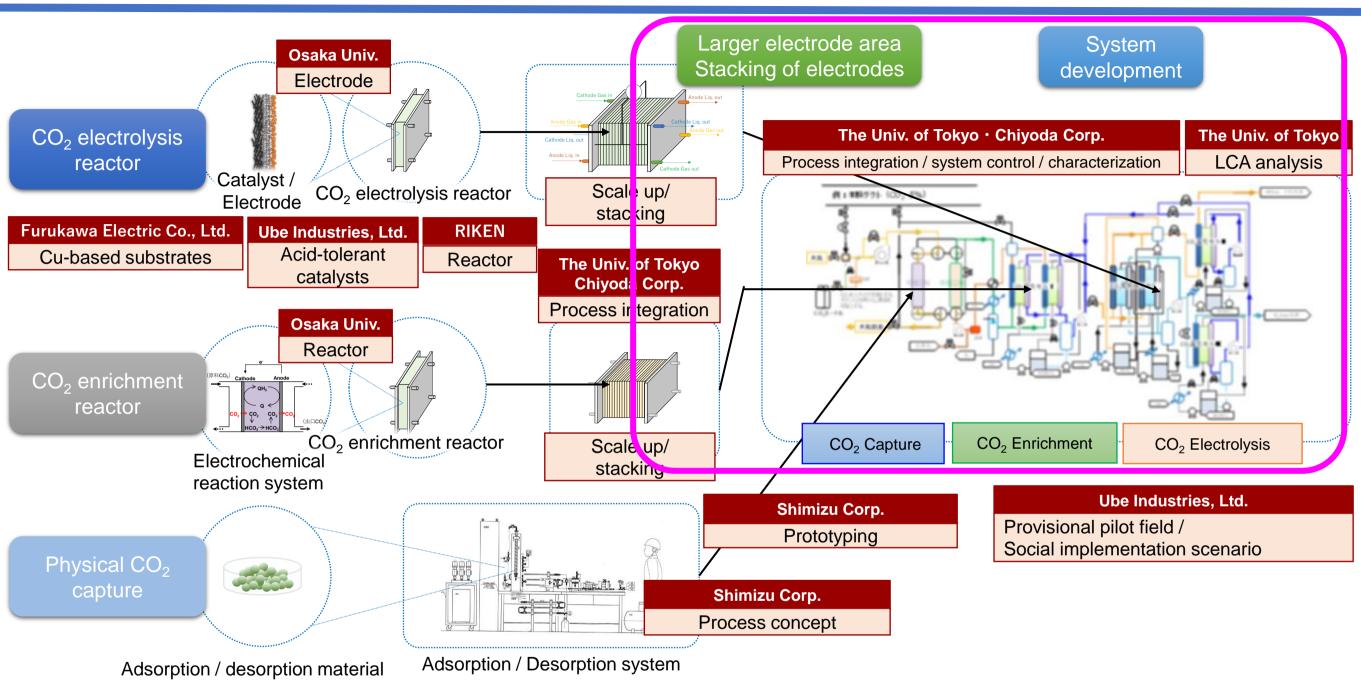
Implementing organizations: The University of Tokyo, Osaka University, Institute of Physical and Chemical

Research (RIKEN), Ube Industries, Ltd., Shimizu Corporation,

Chiyoda Corporation, Furukawa Electric Co., Ltd.

## Project organization and goals





#### Goals

- Development of an integrated system that electrochemically converts CO<sub>2</sub> captured from an atmospheric air to valuable chemical substances
- Conducting a life cycle assessment on a pilot-scale plant to evaluate the effectiveness as a measure against global warming

# Role of the University of Tokyo



#### R&D items

Analysis and control of the integrated system Life-cycle assessment (LCA)

#### Major results so far

- 1) Development of on-line analysis system for CO<sub>2</sub> electrolysis
  - → Product analysis over days with a time resolution of minutes
- 2) Precise potential measurement of a gas-diffusion electrode (GDE)
  - $\rightarrow$  Precise evaluation of the overpotential for CO<sub>2</sub> electrolysis
- 3) LCA for CO<sub>2</sub> footprint on the product C<sub>2</sub>H<sub>4</sub>
  - → Clarification of the blanching point for a carbon-negative process

# **Objectives**



## **□**FY 24

Theoretical design of the operation of DAC, electrochemical  $CO_2$  enrichment, and  $CO_2$  electroreduction in series connection is completed.

Verify the feasibility of a lab-scale system consisting of an electrochemical  $CO_2$  enrichment device and a  $CO_2$  electroreduction device connected in series. (Target continuous operation time: 1,000 hours, current density: 200 mA/cm<sup>2</sup>, a current utilization efficiency: 50%)

LCA evaluation considering a wide range of process conditions.

## **□** FY 27

Prospects for 5,000 hours of continuous operation on a laboratory scale at a current density of 200 mA/cm<sup>2</sup> and a current utilization efficiency of 80% for the product will be determined. Also, obtain the necessary specifications for the pilot design.

LCA evaluation based on the pilot plant design is completed.

## 1) Development of on-line analysis system for CO<sub>2</sub> electrolysis





Current: up to 2 A

• Electrolyte flow:  $0\sim100$  mL/min

•  $CO_2$  flow:  $0\sim 100$  mL/min

• Reaction temperature:  $0\sim80^{\circ}$ C

**Gas product analysis:** 

2 minutes/analysis

**▶ 1 ppm~100%** 



Agilent 490 Micro GC

• 2 channels

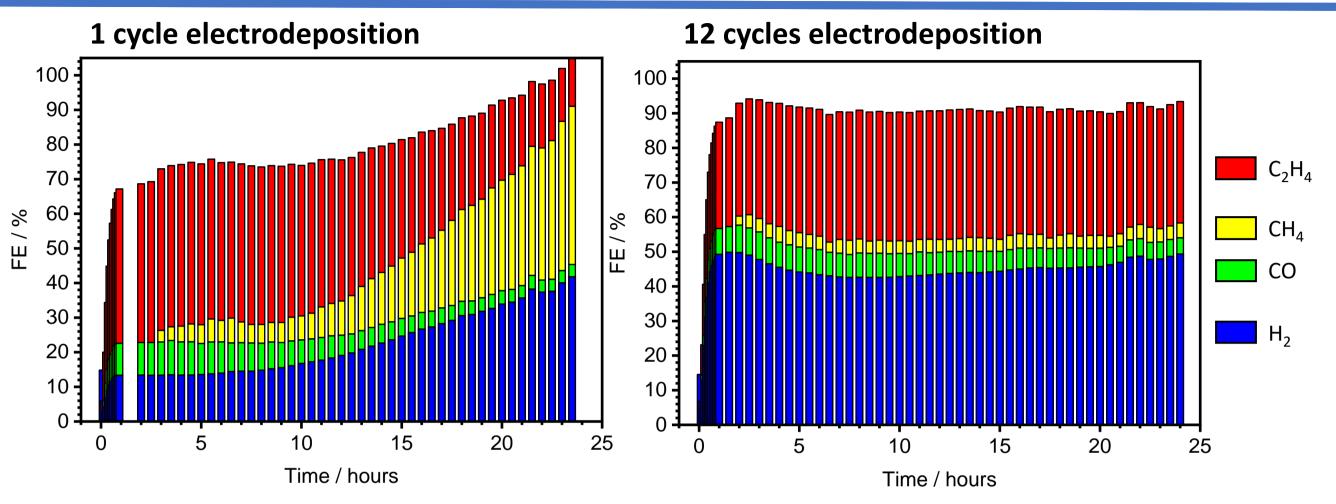
Ch1: Ar, MS5A + Buckflush

Ch2: He, Pora Plot Q

Detectors: MicroTCD

## Ex) CO<sub>2</sub> reduction using electrodeposited Cu<sub>2</sub>O electrode





#### **Deposition amount:**

Small  $\rightarrow$  High initial  $FE_{C2H4}$ , poor durability

Large → Low initial FE<sub>C2H4</sub>, better durability

Development of electrodes for both initial performance and durability.

➤ Necessity for novel analysis and materials

# 3) Integrated system design



#### Collaborative work with Chiyada corporation

Enrichment

Cell

1-1 CO, Capture 1-2 CO, Enrichment (2) CO<sub>2</sub> Electrolysis Separation/purification H<sub>2</sub>+CO H<sub>2</sub>+CO+CO<sub>2</sub>+C<sub>2</sub>H<sub>4</sub> Air **(E)** (E) Separati (E) on/purifi **Ethylene** (CO<sub>2</sub>)Enrichment cell III cation  $C_2H_4$ 

Enric<mark>h</mark>ment

Cell I

 $(co_2)$ 

 $(co_2)$ 

Adsorption / Desorption
Switching

 $CO_2$ 

Adsorption

Exhaust

 $CO_2$ 

Desorption

 $(co_3)$ 

 $\square$  Design of a system flow that integrates the elemental processes under development, from CO<sub>2</sub> capture to ethylene production.

Electrolyzer

■Material balance and heat balance are examined.

H<sub>2</sub>O

 $(CO_2)$ 

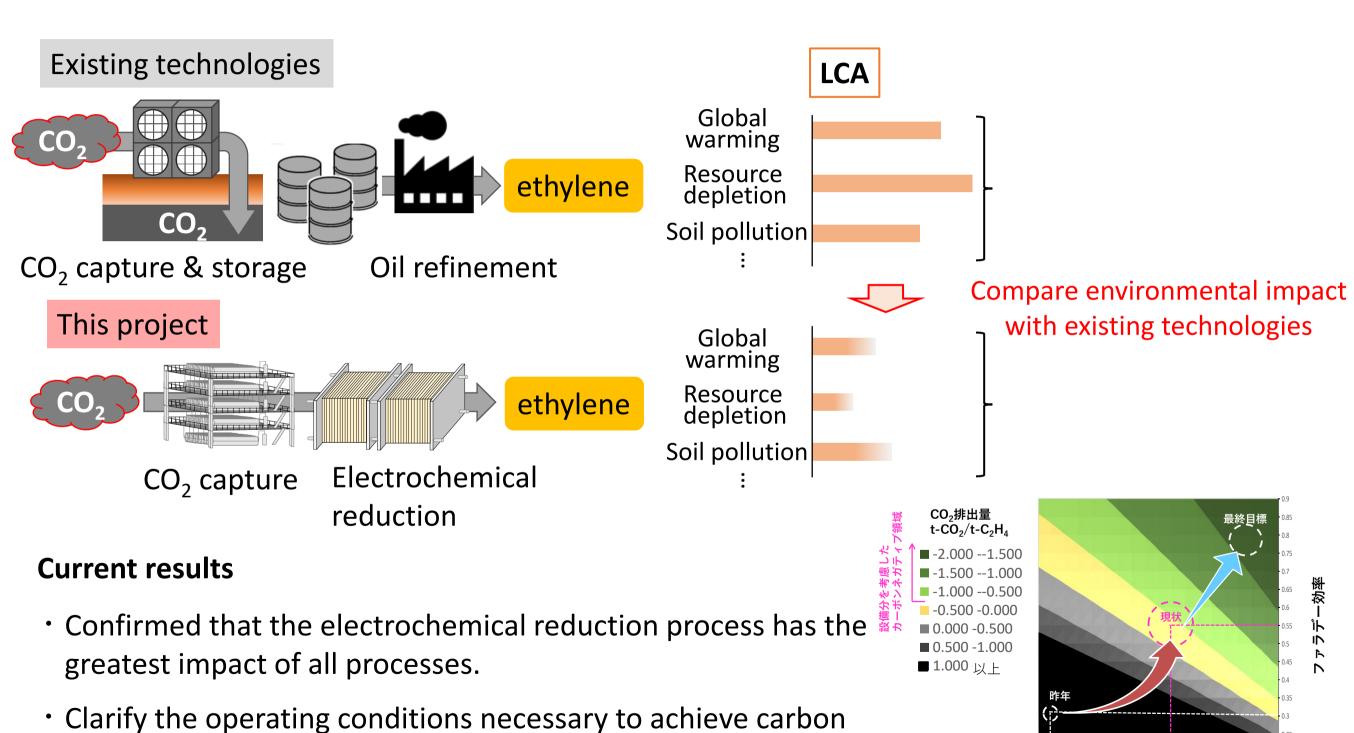
☐Basic Study of LCA

# 3) LCA

negativity ( $CO_2$  emissions  $< CO_2$  fixation)



Integrated assessment of the environmental impact from production to disposal.



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